



ChemPID

Setting the Standard for Automation™

Spring Newsletter 2012

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Upcoming Events

4-8 June	58th International Instrumentation Symposium (IIS)
9-12 June	2012 ISA Spring Leaders Meeting
15 August	7th ISA Marketing and Sales Summit
22-25 September	2012 ISA Fall Leaders Meeting

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Business Unit Manager
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(770) 829-6500

Message from the Director



CHEMPID is charging forward with revised division purpose, Collaborating with ISA divisions and expanding social media visibility

Dear Fellow Chemical and Petroleum Division Members:

In my last winter newsletter, I introduced the new ChemPID board to you. We have been working tirelessly for the past few months to advance ChemPID's new division purpose, outreach and collaborative activities. The board with inputs and recommendations from several members and ISA leaders reframed the division purpose to accurately reflect our membership's interest. I am including ChemPID's new division purpose and welcome your input on the new direction, vision and mission.

ISA ChemPID Division Purpose (Revised December 2011)

The Chemical and Petroleum Industries Division (also known as ChemPID) is organized within the Industry and Sciences Department of ISA. ChemPID aims to contribute to the professional involved in the processing of chemicals, petrochemicals, petroleum, and natural gas. From raw materials to products ChemPID strives to advance best practices in: Safety, Environmental, Production Efficiency, Operations, Process Control, and Automation.

With Global Competition No Operation can run the same year after year. Your plant is either improving or declining. ChemPID is here to give you the tools you need to improve your plant! Have you ever wondered if someone else has already figured it out? Why re-invent the wheel? The key to success is to capitalize on problems that have already been solved and focus your engineering talent on problems that require innovation!

I hope you support our new direction, your input and feedback is very important to us. I would like you to read our board's bio and know more about our individuals who are working very hard for the ChemPID membership. Everyone in the board has become an active contributors and leaders. We have several board positions open, so please contact one of us to get involved. We will guarantee you a great professional and leadership experience with ChemPID.

Our Social media activities and LinkedIn group has almost doubled since my last message to you. We have had over a dozen discussions on the LinkedIn group that have received great interest from our membership. If you are not in our LinkedIn group, please join us. Do not miss out on the thought provoking discussions in critical subjects of interest in chemical and petroleum industry. Send me a note and I will send you a personal invitation to join our Linked in group. Please do not miss out on the exciting networking opportunity – you may get answers from experts, solve your technical challenge or even find the next career opportunity. **DO NOT MISS OUT – JOIN THE OUR GROWING LINKEDIN GROUP BY CLICKING:** www.linkedin.com/chempid

Collaboration is the key to our success at all levels. I am very happy to report that ChemPID has successfully collaborated with

ISA analysis division (AD), ISA Food and Pharma Division (FPID), ISA Management Division, ISA local and regional chapters. I welcome you to read about what other leaders have to say about ChemPID's collaboration in this newsletter. Please note that we are making ChemPID more popular and accessible for your benefit and professional growth.

We are also sponsoring panel sessions at the 57th ISA Analysis Division Symposium and 58th ISA International Instrumentation Symposium ISA events. Please look for ChemPID members and papers in the following events in California.

April 22-26

57th ISA Analysis Division Symposium
Anaheim, www.adsymposium.org

Jun 2-7

58th ISA International Instrumentation Symposium
San Diego, www.isala.org/iis.html

Jun 9-12

ISA Spring Leaders Meeting
San Diego, www.isa.org/slm

As always we request your candid feedback and participation to enhance our division. Please get involved and feel free to contact the board with your comments and feedback.

Respectfully,

Prabhu Soundarrajan

Setting the Standard for Automation™

GATHER LEARN THRIVE

**at the ultimate conference for automation professionals—
ISA Automation Week: Technology and Solutions Event**

I'll be there to network, learn from technical and business sessions, and meet with my suppliers. See you there!



- Six technical tracks on operational and technical excellence
- 120+ leading suppliers in the Solutions Provider Showcase
- Opportunity to join a behind-the-scenes technical tour at Walt Disney World
- Fun and business-friendly receptions include hospitality vouchers every day
- Full conference registrations include luncheon vouchers every day

www.isaautomationweek.org/2012

ISA Automation Week Partner



ISA Strategic Partner, Test and Measurement



ISA Corporate Partners








24-27 September 2012
Orange County Convention Center
Orlando, Florida USA



Meet your board - ChemPID Board



ChemPID Division Director
Prabhu Soundarrajan

Growth leader for Lumasense Technologies' Gas Sensor Business

Leads development and commercialization of infrared and photo acoustic gas analyzers for the chemical, petroleum, energy, clean-tech, medical, and utility markets.



Division Director-Elect
Matthew Conklin

Senior Systems Engineer at R.E. Mason Company in Charlotte, NC.

Conduct industrial automation projects for Chemical, Pharmaceutical, Nuclear Waste Disposal, Petro-Chemical, and Pulp & Paper

Facilities. Specialize with Emerson's DeltaV Distributed Control System.



Newsletter Editor
Rhonda Pelton

Process Automation Manager at Dow Chemical Company

Develops and implements process automation improvement strategies, to ensure the optimization and of process automation

systems and leads the execution of major process automation improvement projects and initiatives



Webmaster/Social Media Expert
George Robertson



Symposium Chair
Alan Bryant

Senior Engineering Advisor Occidental Petroleum

Alan Bryant has a BS and MS in electrical engineering from the University of Missouri at Rolla. He spent 9 years at Exxon working in oil and gas production in the central U.S. as a control

systems engineer and a facilities engineer. Alan worked for a small consulting firm for a year then as one of the product marketing managers for the Modicon Quantum PLC at Schneider Electric. Alan currently works for Occidental Petroleum as a senior engineering advisor in the automation technology group in Houston supporting Oxy's automation systems globally.

ChemPID Board Open Positions:

Newsletter Editor-Elect

Webmaster/Social Media Expert-Elect

Symposium Chair-Elect



LDAR Symposium 2012

14-17 May 2012
Astor Crowne Plaza
New Orleans, Louisiana USA

Unbiased. Unabated. Unrivaled.

ISA's 12th Annual
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Setting the Standard for Automation™

The Missing Link between Operator Alarms, Process Control and KPI's

Robin Brooks, Alan Mahoney, John Wilson, Na Zhao Process Plant Computing Limited (PPCL), PO Box 43, Gerrards Cross, UK.
Robin_Brooks@ppcl.com

Operating Envelope is one of those phrases that everyone uses and understands until they are asked to describe and define an operating envelope for their process. Then they discover that the words they need just don't exist in English (and probably not in any other language either), that they can't draw a picture of an operating envelope and that even with advanced mathematics they can't describe an envelope of their process with equations. So how have plants managed to operate all these years without being able to know whether they were operating inside or outside of the nebulous and undefined Envelope within which they achieve all of their product and KPI objectives? There are three things that all plants do to a greater or lesser extent...

1. They have defined target operating values or small target ranges for all their primary setpoints from past experience of having achieved good product and KPI results and use process control to maintain operation as close as possible to this target point or inside the target ranges. Quite possibly they could get good results or maybe even better results outside this very small target zone but as no one knows where the boundary of the good-results operating envelope actually is, process control is worked hard to operate very close to the target and to quickly return the process to the target zone in the event of a process disturbance.

Optimising controllers and constraint-pushing controls venture cautiously out of the target zone relying upon feedback of some sort to tell them they have reached a boundary of the good product envelope in the direction that they moved. If this were done often enough and all the 'touch-points' captured it could give some information about the envelope. But a point on the boundary of the envelope may be a better place than the target zone to operate at but is not necessarily the best because most or all processes are non-linear whereas many optimising controllers presume linearity so are unable to see local optima that they pass on their path to the boundary of the envelope.

2. They define Operating Ranges on individual variables and for several variables call the collection an Operating Windows. Operating inside all of the variable ranges and thus inside the window will produce better results than operating outside the window. So an Operating Window is a simplified representation of an operating envelope. An Operating Window is larger than a target zone. It is called a window because the effects of interaction between the individual variable ranges are largely ignored hence they form a rectangle in two variables, a cuboid in three and a hypercube or Operating Box in four or more variables. Useful Operating Windows usually have more than four variables so should really be called Operating Boxes but Operating Windows has become common usage. An Operating Window created without knowledge of the Operating Envelope that it is approximating is very likely to be capable of improvement.

3. They try to place Operator Alarms, as often advised, "at the boundary of where the process normally operates" so that when an alarm annunciates it acts similarly to a level probe on a tank by giving just 1 binary bit of information about the

position of an envelope boundary. But as the position of "the boundary of where the process normally operates" was unknown the alarm limits were placed by trial-and-error methods so may or may not be on the boundary of the intended envelope or even all on the boundary of the same envelope. Operating Envelopes are therefore the missing link between process control, operating windows and operator alarms. Surprisingly, they are relatively easy to find, see, work with and model.

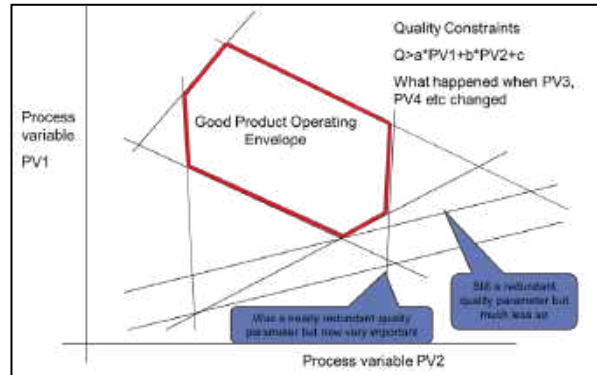


Figure 1, 2-variable cross-section of an envelope

Figure 1 shows in a very simplified form the many constraints that can exist between two process variables that between them outline the red boundary of the 2-dimensional space within which the desired good results may be obtained. But these constraints are functions of many other variables so will move as those other variables change value causing the shape of the red cross-section of the operating envelope to vary with time as in Figure 2 where a third axis has been drawn for time so that we can imagine the operating envelope as a tube of varying cross-section extending through time. But real processes need many more than two process variables to describe their operating envelopes so how can we draw a fourth, fifth, fiftieth and even five hundredth axis at right angles to all the others?

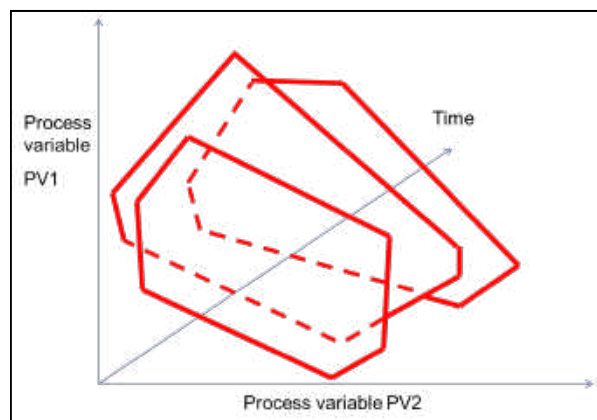


Figure 2, How can more than two process variables be shown?

The answer is don't draw the axes at right angles to each other but draw them parallel to each other instead so that the number of axes is limited only by the width of the paper or the size of the computers memory. This is called a parallel coordinate graph and is actually a coordinate transformation from n-dimensional space

to 2-dimensional space so it has many other mathematical properties. An example is shown in Figure 3. The zigzag line is the transformation of a point from an imaginary 27-dimensional space, where it would have 27 coordinate values instead of the 3 we are used to in our 3-d world. The point is actually the values of all the variables at an instant in time and could have come from the DCS or from the plant historian. It is simple to read and understand but only becomes useful when many points are plotted to form patterns that can be recognised and understood.

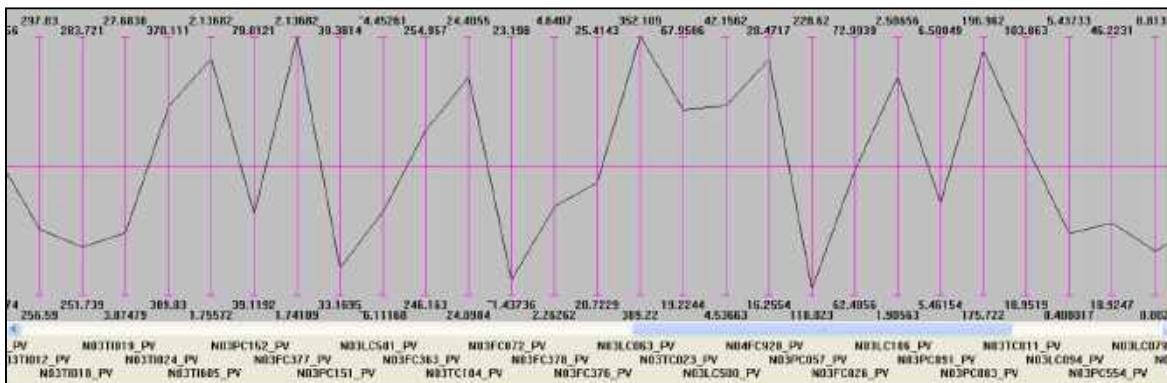


Figure 3, A parallel coordinate graph showing a single point and 27 out of 178 variables.

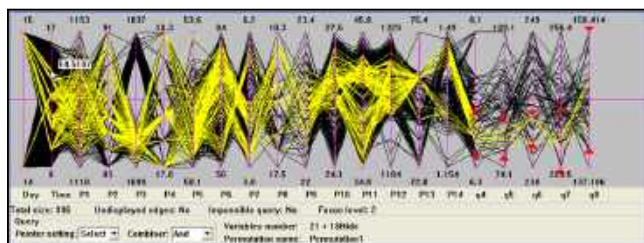


Figure 4, The Operating Envelope for 1st grade product in yellow

Figure 4 shows a simple process with 996 data points at 1-minute intervals. The process variables are labelled P1 – P14. The laboratory analyses of the 1-hour product samples have been joined using sample time as the connecting field and are the q4 – q8 variables.

Finding an Operating Envelope

The product specification for top-grade product is shown as red triangles delineating the allowable ranges of the specifications and all polygonal lines passing through all five ranges have been coloured yellow so it is very clear how the process was operated to make 1st grade product and how it was operated to make something else.

The yellow shape is actually the Operating Envelope for 1st grade product. It includes some prominent non-linearities shown by the yellow bands on P6, P7, P11, P13 and P14 and should be reduced in size before use to exclude the black holes between the bands since there are no process control algorithms available that can recognise and 'jump over' these holes. Non-linearities such as these are not easily seen by other methods.

Finding a Consistent Operating Window

An Operating Window or hypercube uses only the values on the axes of the graph and ignores the information between the axes. In this case it appears the individual process variable operating ranges defining are the solid black ranges on each axis. They are clearly too wide on variables P10 – P13 and too tight on P4 so

form an Inconsistent Operating Window around the operating envelope. The enclosing Consistent Window is easily found by using the yellow ranges on the process variables to define the window and using the selectivity of the individual process variables in achieving the desired result to reduce the number of variables necessary to define the Consistent window to just those from Time (shift changeover procedures were very poor in this plant) to P5 in Figure 5

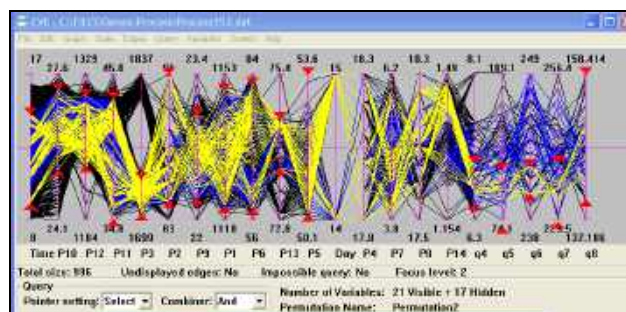


Figure 5, Consistent Operating Window in blue increases yield from 12% to 30%

The Consistent Operating Window encloses all of the yellow 1st grade product points and some additional points from ignoring interactions and not removing black holes but still encloses 39% of the total points including the 12% of yellow points so would give a yield of 1st grade product of 12/39 or approximately 30% if the process was always operated – which is the role of process control - to stay inside the Window. This represents an overnight Yield increase of 250% and is probably achievable without capital investment.

There are many other Operating Windows that are of interest. For instance, the Window on the Manipulable variables can give us information about whether our Manipulable variables are currently capable of controlling to stay within the Window on the process variables or whether and to what extent process control improvements may be needed.

Operating Targets

Even more information can be obtained by comparing operating envelopes as in Figure 6 where a 2nd grade product is shown in blue and super-grade product that is occasionally made almost by accident when everything goes right is in pink. The pink window is probably too small to operate in but gives ranges that can be used as Target Ranges to increase the probability of making super-grade more often in the future. Notice also that the pink window traces a path through the non-linearities showing how they are best avoided.

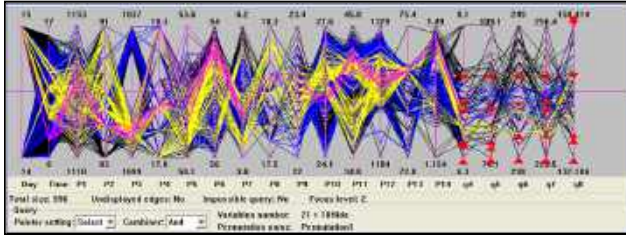


Figure 6, Finding Target operating ranges

All the data behind these graphs has come from existing process history and LIMS databases. The information was always there but just too hard to extract.

Finding Alarm Limits

We need to take enough process operating data from the process historian to adequately represent the range of normal operation with a year being typical so that the annual ambient cycle is covered. Then we import the alarm limits as a query and usually obtain a picture something like that of Figure 7 where many alarm limits are seen to be far outside the envelope of all-operation so can probably never annunciate and others are inside the black area where the process operates so are a cause of false alarms. There is no colour showing that there was at least one alarm visible on the operators alarm list through the whole of the 92 days covered by this data.

Because we started from process history data there we can calculate alarm counts and annunciation rates and show them as conventional time-trends as in Figure 8. These graphs will update as the red triangles are moved so we can interactively adjust alarm settings during the alarm review process and predict the performance they would have given had they been in use during the period of the data. This saves considerable time and debate during the review process and the visibility of the operating envelopes for varying objectives allows the alarm limits to be set

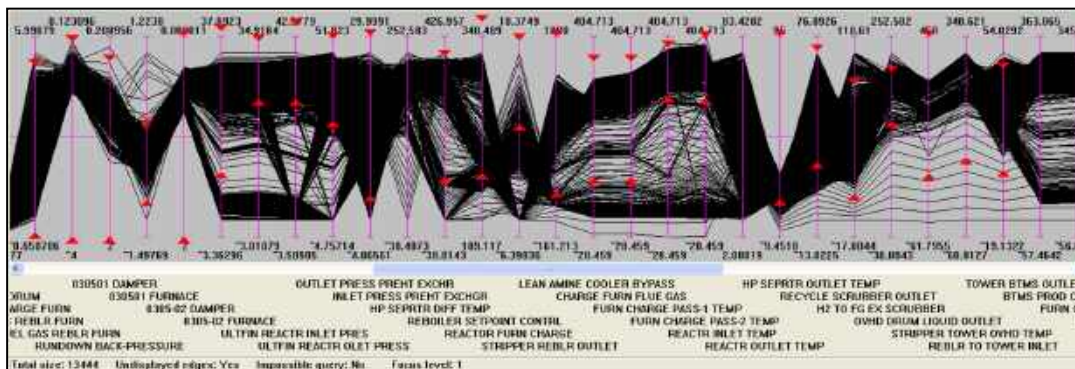


Figure 7, 92 days of operation with at least one alarm present at all times.

much more tightly around the envelope than is possible with other methods to give the operator earlier notification of process excursions with far fewer false alarms yet lower annunciation rates and lower standing alarm counts.

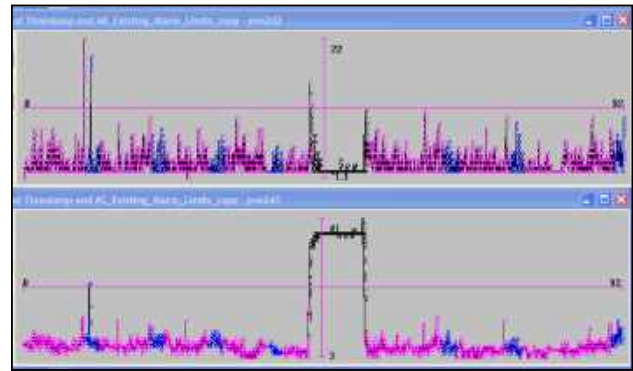


Figure 8, Annunciations/hour (top) and Standing Alarm count over 92 days of operation

Operating Windows, Process Control and Operator Alarm Limits come together in Figure 9 which shows a small number of 178 alarmed variables out of a total of several hundred process variables. The kerosene product operating mode was found using process historian values from an on-line densitometer. Importing the lab analyses of periodic samples and superimposing the product specifications for kerosene gave the turquoise operating envelope. The immediate question was 'why are they different' followed by 'how can they be made the same?' Now that the envelopes and therefore the problem can be seen it is very likely that process control improvements can be made to improve the economic performance of the plant. The control improvements have to be made and be effective before the alarm limits are tightened to capture and lock-in the improvement which is, of course, an on-going process stewardship activity rather than a project activity.

We have seen how to find and use Operating Windows. It is also possible to model the Operating Envelope including variable interactions as a multi-dimensional geometric solid. This is too complex a picture to show statically so a variant display is used to show the process operator in real-time where the process operating point is currently relative to the operating envelope. This real-time variant including variable interactions has many uses including process control, predictive alarming, condition monitoring and prediction of events such as compressor surge and sticking bits while drilling oil wells.

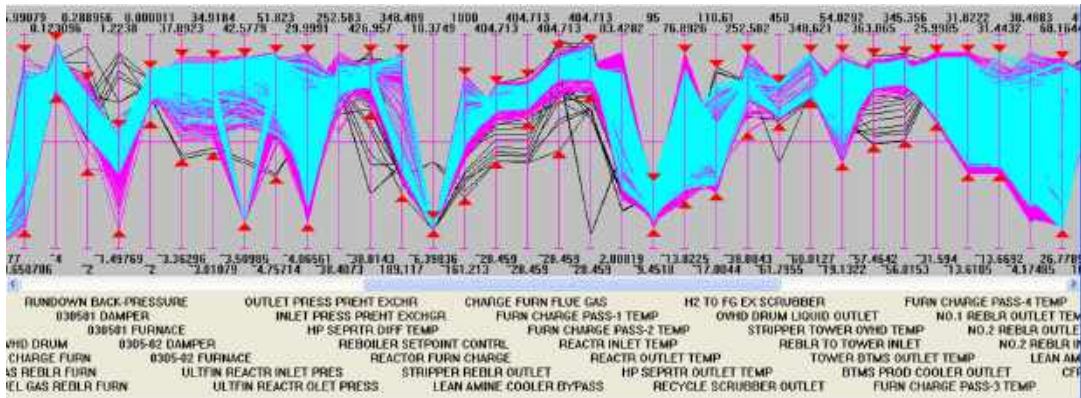


Figure 9, Kerosene Operating Envelope in pink, Best Kerosene Envelope in turquoise.
Why are they different?

CASE STUDY: Ineos Chlor, Runcorn, UK

A Best Operating Envelope was selected and a GPC model built using the real-time C-Process Modeller (CPM). Operator Alarms were reset to the best possible values using existing methods and then benchmarked showing a false alarm rate of 49%. A repeat of the benchmark three weeks after implementing the GPC model had reduced the false alarm rate to less than 10%. At the same time there was a 2% improvement in the efficiency of the process, which does not sound like much but equates to a gain of £700,000 per annum. The start-up time was also reduced by a factor of six, which provided Ineos with one full day extra for production each month.

One of the main advantages of Geometric Process Control for an operating plant is that it is so easy to use, requires no mathematical training and plays to the strengths of the person who knows his process. It is generally predictive of the improved results and alarm performance that can be achieved so does not demand a big leap into the unknown to use its results. Everything stems from being able to see, compare, manipulate, work with and model Operating Envelopes for the first time ever so it is truly a new technology.

More on the results of the Field Trial and on GPC Technology generally can be found on our website www.ppcl.com.

Upcoming ISA Events

57th Annual Analysis Division Symposium

22 – 26 April, 2012

Crowne Plaza Anaheim Resort
Garden Grove, California

ChemPID/FPID Panel: "Integrating analyzers with automation systems for real-time control"

Wednesday, April 25th from 4:30 – 5:00 PM (PST)

Alex Habib FPID Panel Chair

Presenters:

Joseph George of Genentech

David Schilhabel of Oxy

Chris Watts of NNE Pharmaplan

58th International Instrumentation Symposium (IIS)

4-8 June, 2012

Hyatt Regency La Jolla
3777 La Jolla Village Drive
San Diego, CA 92122

ChemPID Paper Sessions

Wednesday, June 6th from 1:30 – 3:00 PM (PST)

Wednesday, June 6th from 3:15 – 3:45 PM (PST)

"Evaluation of Capacitance Sensor for the Liquid Holdup Measurement in Two-Phase with Highly Viscous Liquid"

Authors:

R. Brito, - The University of Tulsa

S. Graham - The University of Tulsa

E. Pereyra - The University of Tulsa

C. Sarica - The University of Tulsa

"Increasing Automation System Security with Better Configuration Management Practices"

Authors: Bill May and Nick Cappi of PAS Inc.

"The Truth About ISA100 Networks & Devices"

Author: Carlo Corso of Honeywell Process Solutions

"Prevention is Better Than a Cure"

Authors: Jo Agar and Gary Fransen of Agar Corporation Inc

2012 ISA Spring Leaders Meeting

9-12 June 2012

Hyatt Regency La Jolla at Aventine
3777 La Jolla Village Drive
San Diego, CA

7th ISA Marketing and Sales Summit

15 August, 2012

The Driskill Hotel
Austin, TX, US

2012 ISA Fall Leaders Meeting

22 -25 September, 2012

Rosen Centre Hotel
Orlando, FL

ChemPID Collaboration Corner

The Food and Pharmaceutical Industries (FPID) and Chemical and Petroleum Industries Division (ChemPID) teamed up for a Panel Discussion at the 57th Annual Analysis Division (AD) Symposium in Anaheim, CA on April 25th, 2012. The theme for this panel is "Integrating analyzers with automation systems for real-time control". The objective is to bring ISA Members together across divisions to share how various industries implement real time analyzer data to control their processes. With presenters from the Biotech and Petroleum fields discussing analyzers and control we hope this panel will lead to more discussions between the three divisions and papers in future symposiums. Thanks to ChemPID for working with FPID! The Analysis Division is pleased to host this joint panel at AD 2012 Symposium and look forward to future collaborations!

- Sandra Krauthamer

The Chemical and Petroleum Division teamed up with the Management Division to improve Social Media Services to its members.

ChemPID thanks Juliann Grant and the Management Division for Social Media Collaboration!

From our collaborative efforts, we have implemented the following actions:

- Strategies to maximize the LinkedIn Group
 - Started a Blog on ChemPID Website and LinkedIn Group
 - Pull in RSS Feed from other industry blogs
- Share articles on a regular basis
- Use Polls to find out what ChemPID Members want from Social Media

Our challenge to the ChemPID membership is to provide feedback on what you want from Social Media and to start discussion of your own.

ChemPID Networking – JOIN the Discussion on ChemPID on Linked In!

Hot topics on ChemPID Linked in:

Should the people who design and implement your process control system be licensed professional engineers? Why or why not?

Alarm Me and Interlock Me at the Same Time

Find the Golden Egg in Your Batch System

Upgrading your DCS

This post was published to Emerson Process Experts at 4:23:26 PM 2/8/2012

Communications Key in Control System Migration Justification and Approval

Account

At a recent conference, Momentive's Brooke Robertson was a presenter on a Control System Migration panel. She described their process to arrive at a global control system modernization decision—from the motivations to the justification process, internal communications, and results.

The motivation for change was control system obsolescence and increasing support costs. This situation increased the risk of extended downtime from hardware failures. Given the constant march of technological advancement over time, control system computing capability was also limiting ongoing optimization efforts.

Other motivations included the desire to standardize control system technology across all global plants to leverage in house expertise for projects and ongoing lifecycle support and gain favorable commercial terms. These motivations together pointed to the need for modern control systems to meet business goals.

Brooke provided many key takeaways for process manufacturers in describing the justification process that they used. It started with developing a vision for the project. This process involved working with the stakeholders from operations, engineering, and plant management to align on the scope, considerations for the risk assessment, and overall project roadmap. Using six sigma-based tools, stakeholders evaluated and prioritized what was important from their individual perspectives. The results of this process not only facilitated communications, it also helped to create a shared vision throughout the organization.

An important part of this process was pictures to help tell the story. One chart that proved to be very effective was an analysis of the age of the control and instrumentation ranked from state of the art to past due versus timeline to repair from hours to months. This helped visually convey the risk of remaining with the status quo.

The output from the stakeholder prioritization process was a customer/vendor matrix of requirements that was provided to the automation suppliers in the request for quote phase. A global team was assembled to review how the suppliers met the elements in the customer/vendor matrix. Initial polling was done to see if a clear supplier emerged from the responses and review process—unfortunately, the views diverged greatly. Through the course of discussions and clarifications, a unanimous decision was reached that was global in scope.

The process that facilitated global stakeholder communications also was effective in receiving full board support for the entire scope of the modernization effort. Projects are now underway, and processes being developed to have collaborative communications channels for engineers, operators, and maintenance teams to share their skills across the organization.

Brooke highlighted the major lessons learned were to involve the senior management team early in the process, open and sustain channels of communications with the stakeholders throughout the vision setting and vendor selection process, and clearly define and communicate the process to the vendors so that expectations were clear.

If you're facing similar issues with obsolescence, increasing support costs, and system limitations to optimization opportunities, perhaps you can apply some of these practices to successfully navigate your organization.

Welcome new CHEMPID members!

Aaron Rodgers

Bishop State Comm Coll

Abdulrahman Saleh Al-Ejji

Dolphin Energy
Instrumentation Reliability Engineer

Ahmed Emam**Alejandro Alvarez Vazquez**

Instituto Tecnológico De Ciudad Madero

Alessio Biasin

RealControl

Alex Dos Santos

Yokogawa America Do Sul
Supervisor De Treinamento

Alyson Tanner

ITI Technical College

Amanda Lucarino

Detection and Measurement Systems Inc
Regional Sales Manager

Andre Henrique De Paula

Translation Design
Coordenador

Andrew Vignes

Real Time Data Application Specialist

Angel Roberto Menjivar Calderon

La Geo SA de CV
Geocientista Jr

Anthony Vance Fiosenzier

INVISTA
Process Engineering Supervisor

Ardell Walters

Kelly Engineering Resources
Sr Recruiter

Augusto Gomes

Stonel
Gerente De Vendas

Ben Thomas

Instrumentation SME

Blaine A. Ford

Bishop State Comm Coll

Blair Adam Hargrave

Sowela Technical Community College

Blake Colin Smith

Sowela Technical Community College

Bruno Alexander Felix Bezerra

Invensys Operations Management
Engenheiro De Instrumentacao

Bruno Mendes Valle

ThyssenKrupp CSA
Tecnico Em Automacao

Carl Scrivner**Carlos Córdoba**

Ingenia S A De C V
Director De Servicio

Carlos Enrique Recinos Ardón

Sherwin Williams De CA SA
Gerente De Calidad

Carlos Hernan Cabrera

Occidental De Colombia
Supervisor Instrumentacion

Carlos Leone Romanholli

Consulat Engenharia
Diretor Técnico

Cesar Augusto Rangel

Occidental De Colombia
Ingeniero Electrico De Facilidades

Charles R. Kelman, ISA84 SFS

INVISTA
Senior Technology Associate

Charlie Brown

Cumberland Valve and Fitting
Regional Sales Manager

Christian P. Bouchard

SK Institute of Science & Tech

Christo Conradie

Lakeside Process Controls
Process Engineer

Christopher D. Rivers

Bishop State Comm Coll

Christopher S. Hebert

Aristotle's Alexander LLC
CEO

Christophor I. Hall

Marathon Oil Company
Instrument Engineer

Clinton Hebert

Sowela Technical Community College
STUDENT

Consuelo Pujaico

Universidad Nacional del Callao

Corey Darensbourg

ITI Technical College
Material Handler

D Angelin

Panimalar Engineering College

Dan Poole

Romatec Inc
Area Sales Manager

Daniel Alves Souza

ThyssenKrupp CSA
Tecnico Instrumentacao E Control III

Danilo Yuri Alves de Lima

UFRN

Danny Emmanuel

Texas State Technical College

Danny J. Soria

Universidad Nacional del Callao

Darcy W. Wright

Aristotle's Alexander LLC
VP of Operations

Darren Taylor

Williams
OpTech III

David Naizer

D&D DesignTech Inc
Co-owner/engineer

David Niedermaier

STUDENT

Demetri Babinsky

Jacobs Industrial Services Ltd
Instrumen Tech 4th Yr Apprentice

Dennis M. Sánchez

Profesional 2

Diego Neves Sá

Engineer

Djoko Rahardjo

petronas
Senior Engineer

Douglas Root

CH2M
EI&C Engineer

Dr. Abhijit S. Badwe

Research Fellow

Dr. Alexey Kozlesov

Tersys LLC
Head of MES Department

Dr. Jose Sergio Rocha Neto

Federal Univ of Campina Grande
Professor

Dr. Julio C. Casquero

Universidad Nacional del Callao
Professor

Dr. Karlene A. Hoo

Texas Tech University
Associate Professor

Dr. Ognjen Kuljaca

Researcher

Dr. Osmar Ogashawara

Universidade Federal De Sao Carlos
Professor Dr Engenharia Eletrica

Dr. Paul W. Murrill

Gulf State Utilities

Dr. Roger Hutton

Crowcon Detection Instruments
Head of Research

Dr. Sérgio LUCENA Lucena, Sr.

Universidade Federal De Pernambuco
Coordenador De Laboratorio

Dr. William Kohley

Spraying Systems Co
VP

Dustin Lane Landry, Mr

ITI Technical College
Mechanic

Eduardo Freitas

Engineer

Edward R. Nugent

Integrated Process T
Branch Manager

Edwin D. Figueroa

SUN CONST
Electrician

Eiji Murakami

Azbil Korea Co Ltd

Elço Pereira Oliveira, Sr.

Net Campinas
Tecnico Em Eletronica

Erick Salvador Ayala Figueroa

Distribuidores Y Productos SA De CV
Supervisor De Producción

Erin Stout

Oxy
Facility Engineer

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